

Design of Vertical Pressure Vessel Using ASME Codes

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ABSTRACT

While preparing this paper many of companies are subjecting to the hazards resulted from the incorrect design and manufacturing of pressure vessels (leakage or Explosion), those used in the storage of dangerous liquids or pressurized fluids. The main objective of using the pressure vessels are used as containers to contain many of materials such as: liquids, air, gases, chemical compounds and fuel, moreover pressure vessels considered as important prop in petroleum and chemical industries especially as storages for oil and chemical components. The main goal of this paper to shed light on the importance processes of the Mechanical Design and Analysis of Vertical Pressure Vessels, also to give scratch to prevent this hazard using. The used model is very close shape to the used vessels in such companies. The design of vertical pressure vessel is carried out using the American Society of Mechanical Engineers (ASME) Codes. ASME section VIII and Division 1 are normally used in design. Various components of the pressure vessel are designed by calculating the appropriate design factors like thickness of the shell, head, stress analysis etc. to validate the design result the pressure vessel is modelled and analyses in Solid works software. The engineering geometrical drawings and Finite Element Analysis (FEA) have been achieved on the targeted model of Vertical Pressure Vessel by using very moderate computer programs to give results agreed and compatible with correct choose of ASME codes. Throughout this paper, the permissible pressures are very considered as well as determination the wall thickness of the vessel is firm to reach the acceptable maximum stresses. Furthermore, the design of targeted pressure vessel has been achieved under the range of ASME codes and engineering standards to reach the allowable designing boundaries.

Keywords: Pressure vessels; ASME codes; Standards; Maximum stresses; Solid works software.

1 Introduction

Pressure vessels are one of the main equipment those widely used in industrial facilities. The pressure vessels defined as cylindrical or spherical vessels those designed to store or hold pressurized liquids, gases or fluids with a differential pressure between inside and outside.

Usually, the inner pressure is higher than the external pressure, except in some cases. The fluid inside these vessels may undergo a change in state as in the case of steam boiler or may



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combine with other reagent as in the case of chemical reactor. The reservoirs designed such that no leakage can occur, also deal with operational levels of high pressure and high temperatures[1]. The pressure vessels are differ in terms of capacity, heat and pressure, some of these vessels may contain more the half million barrels of crude oil, the temperatures sometimes more than 200 °C specially in asphalt tanks and high viscosity products, the temperatures may slope down to 14°C especially in tanks store hydrocarbons materials such as propane, butane and others, so it is necessary to understand the types of reservoirs and their components as well as the appropriate storage methods[2]. Pressure vessels usually are cylindrical or spherical with semi-spherical covers (domes) and cylindrical tanks. Cylindrical vessels very wide in use and very simple to manufacture and ease in use such as boilers, heat exchangers, refineries ...etc. According to the importance of pressure vessels, many of published researches achieved especially in Designing and Analysis of Stresses on the reservoirs as well as the exact use of designing standards, methods of numerical analysis and the mathematical simulation models to identify different collapse occur on reservoirs.

(Apurva R)[3] and friends have used ASME codes to design and analysis of pressure vessel by using maximum permissible pressure to find the factor of safety to obtain the finest design, furthermore, the Finite method element used to study the stresses distribution those deal to reservoir failure. (B. Thakkar and S. Thakka)[4] are designed and constructed in accordance with ASME codes Section VIII, Division 1 by changing internal pressure values of the vessel to obtain the premium design and determination of critical points of collapse in vessel's body. (V. Kumar)[5] used the ANSYS program to design and analyze the loads on the installation fits of horizontal pressure vessel to determine the high stresses concentration between the stiffeners and the wall of the tank, the results were compared with permissible strain of design. (Maharishi J. Bhatt)[6] Studied the design of connecting the nozzle with the tank wall, also to connect this nozzle with upper or lower cover according to ASME codes Section VIII, Division 1. Generally speaking, this paper includes the steps designing calculations to support the nozzle with the tank body and connecting regions.

2 History of ASME Codes for Pressure Vessel

Pressure vessels store energy and as such, have inherent safety risks. Many states began to enact rule and regulations regarding the construction of steam boilers and pressure vessels following several catastrophic accidents that occurred at the turn of the twentieth century that resulted in large Loss of life. By 1911 it was apparent to manufacturers and users of boilers and pressure vessels that the lack of uniformity in these regulations between states made it difficult to construct vessels for Interstate commerce. A group of these interested parties appealed to the Council of the American Society of Mechanical Engineers to assist in the formulation of standard specifications for steam boilers and pressure vessels. (The American Society of Mechanical Engineers was organized in 1880. As an educational and technical society of mechanical engineers.) After years of development and Public comment, the first

edition of the Code, ASME Rules of Construction of Stationary Boilers and for Allowable Working Pressures, was published in 1914 and formally adopted in the Spring of 1915. The first Code rules for pressure vessels, entitled Rules for the Construction of Unfired Pressure Vessels, followed in 1925. From this simple beginning the Code has now evolved into the present eleven Section document, with multiple subdivisions, parts, subsections, and Mandatory and non-mandatory appendices.

Almost all pressure vessels used in the process industry in the United States are designed and constructed in accordance with Section VIII, Division 1. A pressure vessel is a closed container designed to hold gases or Liquids at a pressure different from the ambient pressure. The end caps fitted to the cylindrical body is called heads. Pressure vessels are used in a variety of applications. These include the industry and the private sector. Steel pressure vessel in the industrial sector, pressure vessels are designed to operate safely at a specific pressure and temperature, technically referred to as the "Design Pressure" and "Design Temperature". A vessel that is inadequately designed to handle a high pressure constitutes a very significant safety hazard. Because of that, the design and Certification of pressure vessels is governed by design codes such as The ASME Boiler and Pressure Vessel Code in North America, the Pressure Equipment Directive of the EU (PED), Japanese Industrial Standard (JIS), CSA B51 in Canada, AS1210 in Australia and other international standards like Lloyd's, Germanischer Lloyd, Det Norske Veritas, Stoomwezen etc. Pressure vessels can theoretically be almost any shape, but shapes made of sections of spheres, cylinders and cones are usually employed. More complicated shapes have historically been much harder to analyse for safe operation and are usually far harder to construct. Theoretically a sphere would be the optimal shape of a pressure vessel.

Unfortunately the sphere shape is difficult to manufacture, therefore more expensive, so most of the pressure vessels are cylindrical shape with 2:1 semi elliptical heads or end caps on each end. Smaller pressure vessels are arranged from a pipe and two covers. Disadvantage of these vessels is the fact that larger diameters make them relatively more expensive. Generally, almost any material with good tensile properties that is chemically stable in the chosen application can be employed. Many pressure vessels are made of steel.

3 Using Method of (ASME Section II & VIII, Div1) Calculation

3.1 Selection of Materials by using (ASME Section II: A,D)

The (Section II: A, D) is used to determine selected materials with full description, it permits to use codes for components with different constructions[3].

The main component of any vessel is metal shells with different dimensions on bottom, top and wall. All these dimensions should be suitable with codes under the authority of the designer himself.

3.2 Design of Vessels by using (ASME Section VIII, Div1)

This code (standard) is used for designing vertical tanks (vessels), according to minimum requirements of design without any failure of tank parts. The specialized code for the vessels those used within range of (0.1 MPa to 20 MPa) and for this range most of vertical vessels are selected [9]. The cylindrical pressure vessel composed of: (Shell – Head – Nozzles – Base support).

3.2.1 Shell Design

The ASME codes presents basic rules while designing shells. It is clear that the thickness of these shells is main consideration, the welding operation on vessels is necessary too. The used thickness equations are:

- In case of circumference stresses (longitudinal welding)

$$\text{Where: } (p < 0.385 SE) \quad t_s = \frac{PR}{SE-0.6P} \quad , \quad P_s = \frac{SEt_s}{R+0.6t_s}$$

- In case of longitudinal stresses (circumference welding)

$$\text{Where: } (p < 1.25 SE) \quad t_s = \frac{PR}{2SE+0.4P} \quad , \quad P_s = \frac{2SEt_s}{R-0.4t_s}$$

Where:

t_s = Shell thickness.

P = Designing pressure.

P_s = Maximum pressure.

R = Internal Radius.

S = Maximum allowable stress.

E = Coefficient of connection of welding.

Note that: E = 1.0 if radiated test is used, meanwhile E = 0.7 is used if non-radiated tests are used

3.2.2 Heads Design

Most of used closing heads are curved to resist pressure, reduce thickness and cost reduction. There are many types of closing heads and mostly used is semi-elliptical head. In this type the

$$\text{base diameter to the high} = \frac{D}{h} = \frac{4}{1}$$

The head cover will consist of two main parts are shown in Figure 1:

Spherical radius = (L = 0.9D)

Radius of the neck = (ri = 0.17D)

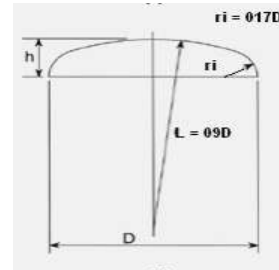
$$t_h = \frac{PD}{2SE-0.2P} \quad , \quad P_h = \frac{2SEt_h}{D+0.2t_h}$$

Where:

t_h = head thickness.

P = Designing pressure.

P_h = Maximum pressure.



S = Maximum allowable stress.
 D = Internal diameter of tank body.
 E = Coefficient of connection of welding.

3.2.3 Nozzles Design

During providing the pressure vessels with nozzles, it is important to support these nozzles to avoid or prevent any failure. The type of nozzle is shown in Figure 2

$$t_n = \frac{PR}{(SE-0.6P)}$$

$$A_r = d_n * t_s * f$$

$$A_s = D_n(T_s - t_s) - 2T_n(T_s - t_s)$$

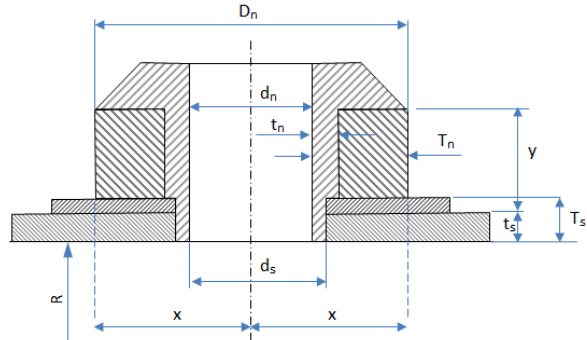
$$A_n = 2[2.5(T_s) * (T_n - t_n)]$$

$$A_r < (A_s + A_n)$$

$$d_s = d_n + 2(t_n)$$

$$x = r_n + T_n, y = 2.5 * T_s$$

$$d_n = D_n - 2(T_n + \text{Corrosion Allowance})$$



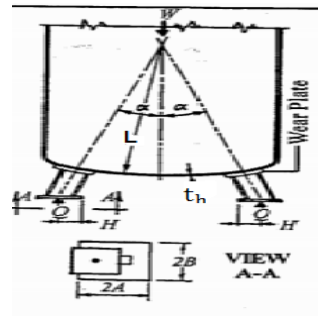
where:

D_n = External nozzle diameter
 d_n = Internal nozzle diameter
 d_s = Diameter of nozzle on tank wall
 f = correction coefficient = 1
 t_s = Required thickness of tank
 T_s = Actual body thickness
 t_n = Required nozzle thickness
 T_n = Actual nozzle thickness
 r_n = Radius of internal hole
 A_r = Area of nozzle hole
 A_s = Area of connecting region
 A_n = Area of nozzle wall

3.2.4 Support Base Design

During designing of high vessels, the support bases, size, volume, weight, wind and earthquake should be taken into consideration. In this work the legs support were used. The support legs are shown in Figure 3. The number of legs depends on the size of the tank and the size of stored material in the tank. The dimensions of the legs and stresses can be calculated as:

- Longitudinal stresses



$$S_L = \frac{Q}{t_h^2} \left[\cos \alpha (k_1 + 6k_2) + \frac{H}{L} \sqrt{\frac{L}{t_h}} (K_3 + 6K_4) \right]$$

- Circumference stresses

$$S_c = \frac{Q}{t_h^2} \left[\cos \alpha (k_5 + 6k_6) + \frac{H}{L} \sqrt{\frac{L}{t_h}} (K_5 + 6K_6) \right]$$

Note that the longitudinal Stress always positive values (k2, k4, k6, k8) mean while the compressional strain (k1, k3, k5, k7) negative values [11].

3.3 Design Calculations and Results

The studied vessel with internal pressure not exceeding (1.55 MPa) and internal temperature not exceeding (100 °C). Table 1 shows the initial material used in vessel.

Table 1: Initial material used in vessel

Part	Material
Tank Shell	SA 515 – Gr 70
Head Cover	SA 515 – Gr 70
Tank Nozzle	SA 106 Gr (B)
Support Base	SA 515 – Gr 70
Support Legs	SA 106 Gr (B)

3.4 Vessel Shell Calculations

Table 2: Properties and dimensions of vessel shell

Internal Pressure	1.55 MPa
Internal Temperature	100 °C
External Pressure	0.103 MPa
Shell Length (L)	4000 mm
Internal Tank Diameter (Di)	1500 mm
Material Type	SA 515 – Gr 70
Permissible Material Stress	137.9 MPa
Link Efficiency	1.0
Corrosion Permeability	3 mm
Density of Material	7.73 g/cm ³

3.4.1 Vessel Shell Thickness

Where:

$$P < 0.385 * S * E = 1.55 < 0.385 * 137.9 * 1$$

$$t_s = \frac{PR}{SE - 0.6P} + c.a$$

$$t_s = \frac{1.55 * \left(\frac{1500}{2}\right)}{(137.9 * 1) - (0.6 * 1.55)} + 3 = 11.48 \text{ mm}$$

(use $t_s = 12 \text{ mm}$)

3.4.2 Maximum Pressure on Vessel Shell

$$p_s = \frac{SEt}{R + 0.6t_s}$$

$$p_s = \frac{137.9 * 1 * 12}{\left(\frac{1500}{2}\right) + 0.6 * 12} = 2.19 \text{ MPa}$$

3.4.3 Vessel Shell Mass

$$Volume = \frac{\pi * (D_o^2 - D_i^2)}{4} * L$$

$$Volume = 228004.22 \text{ cm}^3$$

$$Mass = Volume * Density$$

$$Mass = 228004.22 * 7.73 = 1762.472 \text{ Kg}$$

3.4.4 Liquid Mass at Vessel Shell

$$Volume = \frac{\pi * (D_i^2)}{4} * L$$

$$Volume = 7068583.47 \text{ cm}^3$$

$$Mass = Volume * Density$$

Liquid Density=1.00 g/cm³

$$Mass = 7068.58 \text{ Kg}$$

3.5 Head Calculations

Table 3: Properties and dimensions of head cover

Head cover type	Semi-Elliptic
Internal Tank Diameter	1500 mm
Material Type	SA 515 – Gr 70
Permissible Material Stress	137.9 MPa
Link Efficiency	1.0
Corrosion Permeability	3 mm
Internal Spherical Radius	1350 mm
Head High	375 mm

3.5.1 Required Head Thickness

$$t_h = \frac{PD}{2SE - 0.2P} + c.a$$

$$(use t_h = 12 mm) \quad t_h = 11.44 mm$$

3.5.2 Maximum Pressure at the Head

$$P_h = \frac{2SEt}{D + 0.2t_h}$$

$$P_h = \frac{2 * 137.9 * 1 * 12}{1500 + 0.2 * 12} = 2.2 MPa$$

3.5.3 Mass of Head

$$Volume = \frac{2}{3} * \pi(Lo^2 - Li^2) * h$$

$$Volume = 25559.99 cm^3$$

$$Mass = Volume * Density$$

$$Mass = 25559.99 * 7.73$$

$$Mass = 197.58 kg$$

$$Mass of two heads = 197.58 * 2 = 395.16 kg$$

3.5.4 Liquid Mass at Head

$$Volume = \frac{2}{3} * \pi(Li^2) * h$$

$$Volume = \frac{2}{3} * \pi(135^2) * 37.5 = 1431388.153 cm^3$$

$$Mass = Volume * Density$$

Liquid Density=1.00 g/cm³

$$Mass = 1431.388 Kg$$

$$Liquid Mass of two heads = 2862.776 kg$$

3.6 Nozzle Calculations

Table 4: Properties and dimensions of tank nozzle

Nozzle Length	200 mm
External Nozzle Diameter	203 mm
Material Type	SA 106 Gr (B)
Permissible Material Stress	117.9 MPa
Link Efficiency	1.0
Corrosion Permeability	3 mm

3.6.1 Required Nozzle Thickness

$$t_n = \frac{PR}{(SE - 0.6P)}$$

$$t_n = \frac{1.55 * (\frac{203}{2})}{(117.9 * 1 - 0.6 * 1.55)} = 1.5 \text{ mm}$$

(use $T_n = 10 \text{ mm}$, $t_s = 12 \text{ mm}$ and $T_s = 22 \text{ mm}$)

3.6.2 Nozzle Reinforcement

$$d_n = D_n - 2(T_n + \text{Corrosion Allowance})$$

$$d_n = 203 - 2(10+3), d_n = 177 \text{ mm}$$

$$d_s = d_n + 2(t_n)$$

$$d_s = 177 + 2(1.5), d_s = 180 \text{ mm}$$

$$A_r = d_n * t_s * f$$

$$A_r = 177 * 12 * 1, A_r = 2124 \text{ mm}^2$$

$$A_s = D_n(T_s - t_s) - 2T_n(T_s - t_s)$$

$$A_s = 203 * (22 - 12) - 2 * 10 * (22 - 12), A_s = 1830 \text{ mm}^2$$

$$A_n = 2[2 * 1/2(T_s) * (T_n - t_n)]$$

$$A_n = 2[2.5(22) * (10 - 1.5)], A_n = 935 \text{ mm}^2$$

$$A_r < (A_s + A_n)$$

$$2124 < (1830 + 935)$$

$$x = R_n + T_n$$

$$x = (177/2) + 10, x = 98.5 \text{ mm}$$

$$y = 2.5 * T_s$$

$$y = 2.5 * 22, y = 55 \text{ mm}$$

3.6.3 Mass of Nozzle

$$\text{Volume} = \frac{\pi * (D_n^2 - d_n^2)}{4} * L$$

$$\text{Volume} = \frac{\pi * (20.3^2 - 17.7^2)}{4} * 20 = 1551.95 \text{ cm}^3$$

$$\text{Mass} = \text{Volume} * \text{Density}$$

$$\text{Mass} = 11.99 \text{ kg}$$

$$\text{Mass of two nozzles} = 11.99 * 2 = 23.99 \text{ kg}$$

3.6.4 Total Mass of Pressure Vessel

$$\text{Total mass of vessel parts} = 130.9 + 23.99 + 395.16 + 1762.472 = 2312.5 \text{ kg}$$

$$\text{Total liquid mass} = 2862.7763 + 7068.58 = 9931.36 \text{ kg}$$

$$\text{Total mass (T}_m\text{)} = 9931.36 + 2312.5 = 12243.9 \text{ kg}$$

3.7 Design of Pressure Vessel Support

Table 5: Properties and dimensions of vessel support

Material Type	SA 106 – Gr (B)
Permissible Material Stress on installation sheet	137.9 MPa
Permissible Material Stress on support	117.9 MPa
Link Efficiency (E)	0.6
Number of supporting Legs (n)	4
Spherical Radius (L)	1350 mm
Designed Pressure (P)	55.1 MPa
Lower cover Thickness (th)	12 mm

$$\text{Total mass} = T_m = 12243.9 \text{ kg}$$

$$T_{wf} = 12243.9 * 9.81 = 120112.3 \text{ N}$$

$$Q = \frac{T_{wf}}{n} = \frac{120112.3}{4}$$

$$Q = 30028.1 \text{ N}$$

$$H = 155 \text{ mm} \quad , \quad 2A = 2B = 300 \text{ mm}$$

$$\cos \alpha = 0.95 \quad , \quad c = \sqrt{AB} = 150$$

$$D_L = 1.8 \frac{C}{L} \sqrt{\frac{L}{t_h}} = 1.8 * \frac{150}{1350} * \sqrt{\frac{1350}{12}} = 2.12 \text{ mm}$$

From charts 1,2,3,4 values of K_1 to K_8 can be defined [11].

$$K_1=0.055 \quad K_2=0.02 \quad K_3=0.06 \quad K_4=0.02$$

$$K_5=0.015 \quad K_6=0.01 \quad K_7=0.02 \quad K_8=0.01$$

1.1.1 Calculations of supporting leg dimensions

$$Q = 30028.1 \text{ N}$$

$$E * S = \frac{Q}{A} = \frac{Q}{\frac{\pi}{4}(D_o^2 - D_i^2)}$$

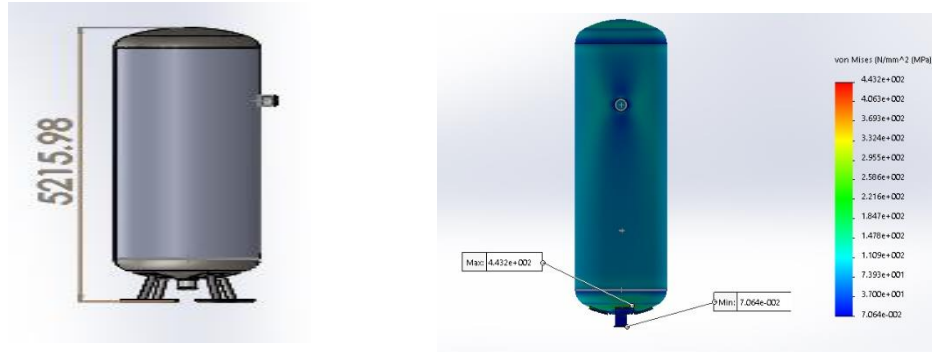
$$0.6 * 117.9 = \frac{30028.1}{\frac{\pi}{4}(D_o^2 - 75^2)}$$

$$D_o = 79 \text{ mm}$$

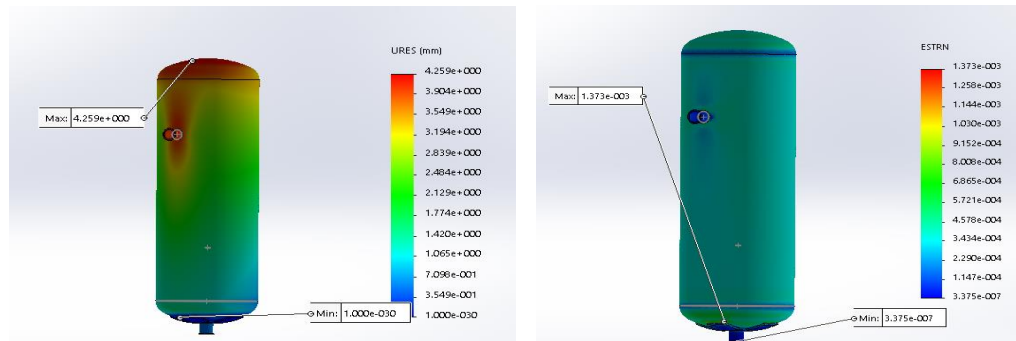
4 Finite Element Analyses

The FE analysis starts with an axisymmetric analysis of pressure vessel. Solid works software is used for the three dimensional modeling of solid structures. The element is defined by eight nodes having three degrees of freedom at each node i.e. translations in the nodal x, y, and z directions. The finite element model consists of hemispherical heads, cylindrical shell and legs support. In boundary condition, the vessel is supported at the end corners and internal pressure of 1.55 MPa is applied at the inner surface. The boundary condition for hemispherical

and end connection pressure vessels are shown in the figure. All parts of vessel have been drawn after finishing all designing calculations. All the drawings drawn by SolidWorks Program. The vertical pressure vessel assembly are shown in Figure 4.



The main purpose of simulation is to determine critical points, stresses concentrations resulted by internal pressure and the distributions of stresses at different regions on vertical pressure vessel with four legs support. The results are shown in Figure 5,6 and 7.



5 Conclusions

It is very clear that the pressure vessels are integrated system in terms of parts and competence. Mechanical design of pressure vessel had been done using SolidWorks software. During the designing of Pressure vessels, it is very important to design each part of these vessels individually to obtain more accurate design. All the pressure vessel components are selected on basis of available ASME standards and the manufactures also follow the ASME standards while manufacturing the components. The designing simulation concludes that the stresses concentration regions concentrated on the regions that connect between the bottom of the tank and the fixing base as well as the regions of fixing of the nozzle on the tank body. Also the designing simulation concludes that the most affected regions to displacement by internal

pressure are the away regions from fixing points (i.e., farther away from installation points the higher displacement value.)

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