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# Effect of Prepration Method on Activity of Ni/Mg/Al Catalysts Prepared From Hydrotalcite Precursors in Dry Reforming of Methane

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### ABSTRACT

The reaction of  $CO_2$  methane reforming was tested over hydrotalcite-based catalysts containing nickel. In order to study the effet of Ni/Mg/Al synthesis methods. Ni/Mg/Al solids were prepared via three ways: (i) coprecipitation at basic pH of Ni<sup>2+</sup>, Mg<sup>2+</sup> and Al<sup>3+</sup> to obtain NiMgAl sample. (ii) MgAl-NiY sample prepared by Chelation-based techniques. (iii) The final way is common impregnation of Ni salts on MgAl hydrotaclite calcined at 450°C and was noted Ni/MgAl. X-ray diffraction (XRD), Brunauere Emmette Teller Method (BET), Temperature Programmed Reduction (TPR), Fourier Transform Infrared Spectroscopy (FTIR), Scanning Electron Microscopy (SEM) were used to describe completely the structural, morphological and surface characteristics of the solids. After reduction at 750°C for one hour, the catalysts were evaluated at the same temperature (750°C), in the dry reforming of methane reaction under continuous flow with CH<sub>4</sub>/CO<sub>2</sub> ratio equal to 1, at atmospheric.

Keywords: energy, methane, hydrotalcite, nickel.

## 1. Introduction

Global warming is one of the major environmental challenges of our time. A major cause of the current global warming trend is the increase in the amount of greenhouse gas released to our environment (CH<sub>4</sub> and CO<sub>2</sub>). Therefore, finding new ways to help tackle and/or reduce the level of greenhouse gas is of paramount importance, this could be achieved by either increasing the use of greenhouse gas (CO<sub>2</sub> and CH<sub>4</sub>) and/or by reducing energy consumption. Catalytic dry reforming of methane (DRM) (also known as CO<sub>2</sub> reforming of methane) converts both CO<sub>2</sub> and CH<sub>4</sub> to syngas (CH<sub>4</sub> + CO<sub>2</sub>  $\leftrightarrow$  2CO + 2H<sub>2</sub>); the reaction has been proposed by many researchers as one of the possible solutions targeted at reducing the amount of CO<sub>2</sub> and CH<sub>4</sub> in our environment. The resulting intermediate is widely applied in the Fischer–Tropsch synthesis, [1-3] to make other value-added hydrocarbons.

## 2. Experimental

Hydrotalcite-derived catalysts were prepared *via* co-precipitation method following procedure previously described. [4] NiMgAl sample catalyst was synthesized with molar ratio  $(nNi^{2+}+nMg^{2+}/nAl^{3+}) = 2$ . In order to study the effect of Ni position in within the NiMgAl hydrotalcite-derived catalysts structure (i.e., in the brucite layer or in the interlayer space of hydrotalcite), we embarked on the synthesis of MgAl-NiY sample using the co-precipitation method reported above with molar ratio  $(nNi^{2+}/nAl^{3+}) = 2.4$ . The synthesis of MgAl-NiY hydrotalcite-derived catalysts layered double hydroxide (LDH) included two steps. Following a procedure previously described [5].



#### 3. Results and Discussion

The diffractograms of the NiMgAl and MgAl-NiY solids both show reflection peaks at  $2\Theta = 60^{\circ}$ , with the same value of d110 (1.51 Å). This suggests that no change in the cation-cation distance in the brucite-like layers has occurred. The lattice parameter calculation gave the value of 3.02 Å which is in good agreement with the literature [6]. The value of parameter c of the MgAl-NiY solid is 44.97Å whereas it is approximately 22.14 Å in the case of the solid NiMgAl. Indeed, the intercalation of [Ni(Y)-2] species between the sheets of brucite led to the extension of the spacing d003 and consequently an increase in the lattice parameter c.

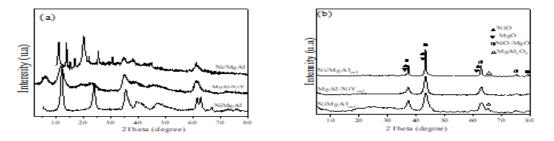


Figure 1: X-ray diffraction diagrams (XRD) (a) for synthesized precursors (b) Respective mixed oxides

The catalytic performance of the different catalysts for  $CO_2$  reforming of methane were evaluated at a reaction temperature of 750°C using a 1/1 of  $CH_4/CO_2$  feed ratio, after an "in-situ" H<sub>2</sub> reduction at 750°C for 1 hour. The main products from this reaction were H<sub>2</sub> and CO. The performances levels of the catalysts remain constant after 8 hours of reaction time, indicating that no or little deactivation took place within this period, at least under the conditions used. If we focus on the CH<sub>4</sub> conversion, we could say that catalysts NiMgAl (ca. 94%) and MgAl-NiY (ca. 78%), followed by Ni/MgAl (ca.61%). The conversion for CO<sub>2</sub> shows a similar tendency: NiMgAl ca. 95.0%, MgAl-NiY (86.0%), Ni/MgAl ca. 76%. for the NiMgAl, presenting almost double conversion for CO<sub>2</sub> (90%) than for CH<sub>4</sub>.

 $H_2/CO$  ratios obtained at 750°C, in presence of Ni based-catalysts. This figure is a direct consequence of the differences in the conversion levels of  $CH_4$  and  $CO_2$  as can be seen, during the test (after 8 h on stream), the value of the  $H_2/CO$  ratio remains approximately constant for all the catalysts. For NiMgAl sample, the  $H_2/CO$  ratio is almost that corresponding to the thermodynamic equilibrium (ca. 1.0). On the other hand, MgAl-NiY and Ni/MgAl shows a  $H_2/CO$  ratio smaller than unity. The deviation from the stoichiometric ratio, the occurrence of the reverse water-gas shift reaction.

#### 4. Conclusions

Different types of catalysts of the type containing Ni/Mg/Al have been prepared by thermal decomposition. The synthesized catalysts were successfully characterized and applied for syngas production from  $CO_2$  reforming of methane at 750 °C. The hydrotalcite structures were confirmed using XRD analysis, while the intercalation of Ni in the interlayer space was verified using both XRD and FTIR. The results also showed that the activity and stability of Ni-based catalysts were related to the Ni positioning; the best catalytic activity was observed with NiMgAl.

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